

# HEAT TRANSFER

- Q1. Consider a hemispherical furnace with a flat circular base of diameter  $D$ . The view factor from the dome of this furnace to its base is
- 2
  - $\frac{1}{2}$
  - 12
  - 4
- Q2. Two very large parallel plates are maintained at uniform temperature of  $T_1$  and  $T_2$  and have emissivities  $\epsilon_1$  and  $\epsilon_2$  respectively. The net rate of radiation heat transfer between the two surfaces per unit area of the plate is \_\_\_\_\_ kW
- Q3. A stainless steel cylinder of inner diameter 18 cm and outer diameter 21 cm. Length is 2m. Has its inner surface at  $900^\circ\text{C}$  and outer surface at  $300^\circ\text{C}$ . The radius when the temperature is  $500^\circ\text{C}$  is \_\_\_\_\_ cm
- Q4. Two very long concentric cylinders of diameter  $D_1$  and  $D_2$  are maintained at uniform temperature of  $T_1$  and  $T_2$  and have emissivities  $\epsilon_1$  and  $\epsilon_2$  respectively. The net rate of radiation heat transfer between two cylinders per unit length of the cylinder is \_\_\_\_\_ kW
- Q5. Find out the amount of heat transfer through iron fin of length 50 mm. Area Atmospheric temperature is  $20^\circ\text{C}$  and surface temperature is  $80^\circ\text{C}$ . Assume  $k = 210 \text{ kJ/m hr}^\circ\text{C}$  and  $h = 42 \text{ kJ/m}^2 \text{ hr}^\circ\text{C}$
- 24.23 kJ/hr
  - 30.61 kJ/hr
  - 51.6 kJ/hr
  - 15.1 kJ/hr
- Q6. After expansion from a turbine, the heat exhaust gases are used to heat the compressed air from a compressor with the help of a cross flow compact heat exchanger of  $[\epsilon = 0.8]$  what is NTU
- 2
  - 4
  - 8
  - 16
- Q7. Two long parallel surfaces each of  $\epsilon = 0.7$  are maintained at different temperatures and have radiation exchange between them. It is desired to reduce 75% of this heat using this parallel sheet  $\epsilon = 0.7$ . The number of sheet required are \_\_\_\_\_
- Q8. The heat transfer coefficient for a gas flowing over a thin flat plate 3 m long and 0.3 m wide varies with distance from the leading edge according to  $h_i(x) = 10x^{(-1/4)} \text{ W/m}^2\text{K}$ . Rate of heat transfer between plate and gas is the plate is at  $170^\circ\text{C}$  and the gas is at  $30^\circ\text{C}$  is \_\_\_\_\_ W
- Q9. Extended surface are used to increase rate of heat transfer when the convective heat transfer coefficient  $[h = mK]$ . The addition of extended surfaces
- will increase the heat transfer rate
  - decrease the heat transfer rate
  - not effect the heat transfer rate
  - first increases and then decreases the heat transfer rate
- Q10. For a thin sheet total  $E = 32 \text{ W/m}^2$ . Total irradiation  $G = 93 \text{ W/m}^2$ . For the given sheet reflectivity  $(\rho) = 0.6$ , absorptivity  $(\alpha) = 0.1$ , Transmissivity  $(\tau) = 0.3$ . Value of radiosity (J) is \_\_\_\_\_  $\text{W/m}^2$